"Get the Design Right, the Rest is Automatic" An Adaptive MPC Technology

Yucai Zhu Tai-Ji Control Best, The Netherlands

Contents

- 1. Introduction
- 2. The Architecture of the Adaptive MPC
- 3. How does it Work?
- 4. Software Implementation
- 5. Application to a PTA unit
- 6. Future Plans and Outlook

1. Introduction

- MPC has brought significant benefits in the refining/petrochemical industry. It has also attracted interests from other industries
- The cost of MPC deployment and maintenance is very high due to its technical difficulties and long plant test time
- An adaptive MPC is introduced to solve the high cost problem
- Using the adaptive MPC, the scarce MPC expert is only needed for controller design
- The commissioning and maintenance can be done automatically under the supervision of the operator
- Nonlinear MPC control is achieved using multiple or LPV models.

1. Introduction (Cont.)

Traditional Project Approach to Industrial MPC

- 1. Controller design and benefit study (10%)
- 2. Pre-test (10%)
- 3. *Plant (step) test and model identification (40%)
- 4. Controller simulation and tuning (15%)
- 5. Controller commissioning and operator training (25%)
- 6. *Controller maintenance (mainly re-identification)

- 2. The Architecture of the Adaptive MPC
- Integration is the philosophy behind the technology there are **three** modules in the adaptive MPC



- Online automatic (open and closed-loop) identification and automatic controller tuning make the adaptation possible
- Steps 2 to 6 can be performed automatically

2.1 Online Identification Module

- Testing device
 - Perform automated multivariable test
 - Test can be open loop and/or closed-loop
 - Data collection
- Model ID device
 - Automated data pre-processing and model identification
 - Automated model validation and selection
 - Send good models to MPC Controller Module

2.2 MPC Controller Module

MPC parameter auto-tuning

- Dynamic control parameters can be auto-tuned
- Auto-tuning based on the model and data
- Tuning aims at good and robust control, though not optimal
- Economic optimization parameters are given in design

MPC control algorithms

- Steady state optimization: priorities, weights, IRV, LP&QP
- Dynamic optimization/control: QP, CV reference curve
- Can change model dynamically, necessary for nonlinear MPC

2.3 MPC Monitor Module

- Monitor CV variances for control performance
 - CV variances are compared to their benchmark variances
 - CV setpoint changes are excluded in the calculation
- Monitor MV/CV on/off status for control performance
- Monitor CV simulation error variances for model quality
 - Error variances are compared to their benchmarks
 - Test signal (excitation) may be used.

3. How Does the Adaptive MPC Work? <u>MPC Commissioning</u>

Given an MPC design for a process unit:

- Set up the communication between the DCS and the PC
- Start identification test and online identification; models are created automatically at a given interval or by a mouse click
- Good quality models will be used in the MPC controller while test is ongoing
- When most (or all) expected models are with good quality, the plant test is stopped and the MPC is commissioned.

3. How Does the Adaptive MPC Work (Cont.) ? <u>MPC Maintenance</u>

- MPC Monitor continuously monitors the MPC performance
- When model mismatch becomes too large, the MPC Monitor will activate online identification in closed-loop
- Models are created automatically at a given interval or by a mouse click
- Good quality models will replace the old ones in the MPC controller while test is ongoing
- When most or all poor models are identified and replaced, the maintenance is done.

3. How Does the Adaptive MPC Work (Cont.) ?

The Old Way: Series steps, 3 to 4 software packages

Pre-test Step test & model ID	Simulation	Commission
-----------------------------------	------------	------------

The "New" ID: Series steps, 3 to 4 software packages

Test & model ID	Simulation	Commission
-----------------	------------	------------

The New Way: Parallel procedure, 1 package

Test & model ID

Simulation

Commission

4. Software Implementation

- Two modules are implemented: Controller and Identification
- Can use multi-model and LPV model for nonlinear MPC.



Configuration: Specify general items

🔽 TaiJi MPC - C:\TaijiMPC1.17\TaiJiMPC\bin_NEW0.ojp		
File View Tools Help		
D 😅 🖬 🐚 🎒 💡		
Configure ID Test Model ID Controller Simulation Controller		
General MVs DVs CVs Expectation		
Datasource OPC CIMIO PHD OTHER Remote host name OPC server name PSII.OPC.1	Times Sampling Time: 1 minutes Time to steady state,4*tau: 120	
MV Extention OP SP .OP .SP PV MODE .PV .MODE MV' writable mode(use semi-colon delimited list, * always enable wrote) *	Watch dog Enable DCS start MPC Use watch dog Enable Value Enable 180 Tag name MPCWATCHDOG MPCSTARTCONTROLLER	
OCS MPC Interface Extention Scheduler Control ON/OFF ON/OFF STATUS ON/OFF STATUS	Options Options Image: Automatically start identification model ID interval(>=60 min) 120 Image: Automatically use model in controller	
HEIGHT(MV_CV) LOW(MV_CV) I-HI I-LO STEADY STATE(MV_CV) SETPOINT(CV only) I-TARGET I-SETPOINT	Clear older model in controller ✓ The plant is a real process. Time Compression Factor(>=1)	
teady		

Configuration: Specify MVs, DVs and CVs

🖅 Tai Ji	MPC = C:\Tai=	Ji MPC 1.0\I	emo\ShellMod	lel.ojp						EN	2
<u>F</u> ile	<u>V</u> iew <u>T</u> ools	<u>E</u> xpotr Mod	el <u>H</u> elp							. — .	
D 🚅	; 🔲 फि 🚑	\$?									
Config		Model TD	Controller	Simulation	Controller						
	ue ib iest			- Similarion	controller						
Ger Ger	ierai mys		CVS	Expectation							
MVs	MVs Madd X Del 🕈 Move up 🗲 Move down										
	MV tag name		Hight limit	Average	Low limit	Current	value A	mplitude De	scription		1
1	MV1		5	3.509	-5	3.509	1				
2	MV2		5	1.6	-5	1.6	1			1	
3	MV3		5	1.807	-5	1 807	1			-	
3	1403		5	1.007	-5	1.007	1				
🤝 Tai Ji	i MPC - C:\Tai	-Ji MPC 1.0	\Demo\ShellM	lodel.ojp						- 🗆	E
<u>F</u> ile	<u>V</u> iew <u>T</u> ools	Expotr Mo	del <u>H</u> elp								
 D 📬	 2 🖾 Bra 4	 3, 92									
		≝″8 ∎. 3.7 TD	L C		L C 411 - 22 - 11	1					
Lonrig	re ID lest	model ID	Lontroll	er Simulation	Lontroller						_
Gei Gei	neral MV	s DAR	UVs I	Expectatio	on						
DVs	ど	Add	< Del	🕈 Move up	🗲 Move do	wn					
	DV tag name		C	urrent value		Descrip	tion				-
1 DV1 -0.6788							7				
2	DV2		0.	.2222							
	_										
🆅 Tai Ji	MPC = C:\Tai=Ji	MPC 1.0\Demo	ShellModel. o	ip					EN 21 -	- 0	×
<u> </u>	<u>V</u> iew <u>T</u> ools	<u>E</u> xpotr Model	Help								
] 🗅 🚅	🖬 🗈 🥔	ę									
Configu	re ID Test	Model ID C	ontroller Sim	ulation Contr	roller						
Gen	eral MVs	DVs	CVs Exj	pectation							
CVs	ba 🔛	d 🔀 De	1 🗲 M	ove up 🗲 🖡	Move down						
	CV tag name	Hight limit	Low limit	Current value	MV-VALV/No delay	Integral	Calculated	Calculated function	Description		
1	⊂V1	0	-5	-33.82			<u> </u>				
2	CV2	5	-5	-40.23							
4	CV4	20	-20	-9.636							
5	CV5	20	-20	-1.588							
6	CV6	20	-20	-6.838							
7	CV7	5	-5	-28.07							
Beady											

Configuration: Specify Expectation Matrix

🚰 TaiJi MPC - C:\Tai-Ji MPC 1.0\Demo\ShellModel.ojp 📃									
<u>F</u> ile <u>V</u> iew <u>T</u> ools <u>Expotr Model H</u> elp									
Configure ID Test Model ID Controller Simulation Controller									
General MVs DV	s CVs	Expectation							
	MQ1.	MU2,	MUQ,	DV1.	DV2-				
	MV1	MV2	MV3.	DV1. DV1	DV2: DV2				
CV1:CV1	+	no	+	?	+				
CV2:CV2	+	+	+	+	+				
CV3:CV3	+	+	+	+	?				
CV4:CV4	+	+	+	+	+				
CV5:CV5	+	?	+	+	+				
CV6:CV6	+	+	+	+	+				
CV7:CV7	+	+	+	+	+				
Ready									

ID Test, MV plots



Model step responses



Controlled CVs:

ID test on; 2) ID test stopped; CV1 and CV2 changed setpoints



5 Application to a PTA Unit

1) Solvent Dehydration Tower

Controller commissioned after 10 hours of test



MV Signals during plant test



Model step responses

🚾 Taiji MPC - C:\H701D401\H701D401.ojp										
<u>F</u> ile <u>V</u> iew <u>T</u> ools <u>Export Model H</u> elp										
Configure	Configure ID Test Model ID Controller Simulation Controller									
MVs & DVs CVs Model Response Delay Gain										
1TC17	01.SP	1FC1702. SP	1FC1411.SP	1FC1412. SP	1FI1614. PV	1FI1615. PV	1FI1703. PV	1FI1704. PV	1LS1301. PV	
Ad : TOL IIII 9.851	B	- В 5.899е-002	No model!	No model!	? D 9. 463e-002	? D -4.821e=002	? D 4.889e-002	? D -1.794e-002	No model!	Use expectation matrix Auto estimate delay
. PV	Å				<u> </u>	? D	? D	<u>}</u>		Identify
-1.	973	0. 1841	No model!	No model!	0. 5894	-0.3152	-0. 3286	0.2433	No model!	Layout
PV +	В	+			? D	? D	? D	? <u>D</u>		Cvs jo
IPD1701.	7796	0.2551	No model!	No model!	0.325	-0.5208	3.489e-002	0.3607	No model!	MVs 9
8 ?	в	? D				? D	? D	? D		Plot type
0.3	3175	0. 5776	No model!	No model!	No model!	0. 1631	0. 576		No model!	 Step & Freq. Re Step Resp. Freq. Resp.
8										C Simulation
и ом 1FV1702.	odel!	Mm-0.688	No model!	No model!	No model!	No model!	0.1405	No model!	No model!	Step Resp.
2		<u> </u>							? B	
1011401. Иом Иом	odel!	No model!	1.604e-002	1.445e-002	No model!	No model!	No model!	No model!	-0. 1281	Zero Line
1Q11402. FV	odel!	No model!	<u>В</u> 1. 49е-002	1.66e-002	No model!	No model!	No model!	No model!	? <u> </u>	Plot length 300
ITII731. PV	B 925	0.4832	No model!	No model!	No model!	No model!	? D 0.4274	No model!	No model!	
Ready	Ready X:0 Y:0									

CV responses after MPC turned on



5 Application to a PTA Unit (Cont.)

2) Reaction Section

- MPC has 16 MVs, 1 DV, 18 CVs; 3 x 10 hour tests used
- Control OK; some closed-loop test/ID can improve model quality







MPC off

MPC on

5. Future Plans and Outlook

- Add MPC monitor module
- Add Internet access capability
- Our vision:

An MPC controller is designed by a control expert and it can be implemented and maintained by an operator

- An adaptive MPC is justified for **all process units** in the refining/petrochemical industry, not just major units
- An adaptive MPC is justified for **all process industries**, not just the refining/petrochemical industry.